

Uptake of NO₃ on Water Solutions: Rate Coefficients for Reactions of NO₃ with Cloud Water Constituents

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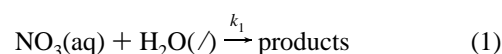
The reactive uptake coefficients, γ , of NO₃ onto aqueous solutions containing ions X⁻ = HSO₃⁻, SO₃²⁻, HCOO⁻, CH₃COO⁻, and OH⁻ were measured at 273 ± 1 K using a wetted-wall flow tube reactor. The values of H^2D/k (H = Henry's law coefficient, D_l = diffusion coefficient in the liquid phase, and k = second-order rate coefficient for the liquid phase reactions of NO₃ with X⁻) for the reactive uptake of NO₃ were determined by measuring γ as a function of liquid phase reactant concentration. The linear correlation between the measured rate coefficients and those for corresponding SO₄⁻ reactions, and the dependence of the measured rate coefficients on the redox potential of the X/X⁻ pair suggest that the NO₃ + X⁻ reactions proceed by electron transfer. The atmospheric implications of these findings are briefly discussed.

Introduction

The nitrate radical, NO₃, formed primarily by the reaction of NO₂ with O₃ in the gas phase, is an important nighttime gas phase oxidant in the atmosphere.^{1,2} The NO₃ radical can also be an important nighttime oxidant in atmospheric droplets and aerosol,^{3–6} which contain dissolved species such as SO₂, HSO₃⁻, SO₃²⁻, organic acids (such as formic acid, acetic acid), and halides (in the marine boundary layer).^{7–9} The liquid phase reactions of NO₃ with these species can initiate the catalytic oxidation of S(IV) via the formation of radical species such as OH, SO₃⁻, and Cl₂⁻.^{3,4,6} The uptake of NO₃ into cloud droplets and aerosol is governed by its solubility, liquid phase diffusion, and reactions in the liquid phase. Therefore the rate coefficients for the reactions of NO₃ with the constituents mentioned above, under atmospheric pH and salt concentrations, are needed to assess the role of the heterogeneous reactions of NO₃ in the troposphere.

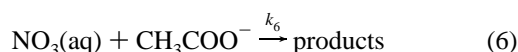
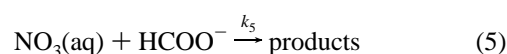
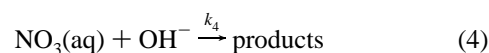
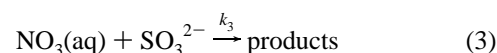
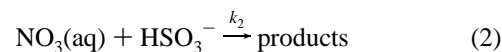
Second-order rate coefficients for the reactions of NO₃ with several ions have been measured in the bulk liquid phase.^{10–14} However, the agreement between the rate coefficients measured in pulsed radiolysis^{11,12} and laser photolysis studies¹³ is poor for some reactions. For example, the rate coefficient for the reaction of NO₃ with Cl⁻ measured using laser photolysis¹³ is about an order of magnitude smaller than those obtained by pulsed radiolysis studies.^{11,12} This disagreement was attributed to the ionic strength effect on the neutral-ion reaction.¹³

Recently, we initiated studies on heterogeneous chemistry of NO₃. In previous papers,^{15,16} we reported the reactive uptake coefficients of NO₃ on water and some ionic solutions and proposed that NO₃ was taken up irreversibly by liquid water due to reaction 1:



NO₃ uptake was found to be controlled by reactive losses in the liquid phase. Furthermore, the rate coefficients for the reactions of NO₃ with halide ions in solution increase with decrease in redox potentials.

In this paper, we report the relative rate coefficients for the liquid phase reactions of NO₃, reactions 2–6, obtained by measuring uptake coefficients of NO₃ into aqueous solutions using a wetted-wall flow tube reactor:



A possible mechanism for the liquid phase reactions of NO₃ and the atmospheric implications of these results are also discussed.

Experimental Section

A wetted-wall flow tube reactor was combined with NO₃ detection through a long-path 662 nm absorption to measure its uptake coefficients onto aqueous solutions. The details of the experimental setup were described previously.^{15,16} Briefly, NO₃ was generated by thermal dissociation of N₂O₅ in an oven maintained at 400 K and was introduced into a flow reactor (i.d. = 1.9 cm) through a movable injector (i.d. = 0.53 cm). NO₃ was detected by measuring its absorbance at 662 nm (from a tunable diode laser) in a long-path White-type absorption cell (optical path length = 1260 cm). The initial concentration of NO₃ used in this work was in the range of (2–20) × 10¹¹ cm⁻³.

The flow rates of the liquid film were in the range 1.3–4 cm³ s⁻¹. The thickness and the flow velocity of the liquid film

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were calculated to be ~ 0.025 cm and ~ 10 cm s⁻¹, respectively. To minimize evaporation of water from the liquid film, water vapor from a saturator was added to the main He flow. The flow velocity of the carrier gas was varied between 500 and 1600 cm s⁻¹. All experiments were performed at 273 ± 1 K and at a total pressure of 10–16 Torr.

Reagent grade chemicals, NaCl, NaOH, NaHSO₃, Na₂SO₃, HCOONa, CH₃COOK, and NaNO₃, were used without further purification. The solutions were prepared using deaerated deionized water (>17.5 M Ω cm). The concentrations of formate and acetate ions from the weak acids, formic and acetic acids, were calculated using the pH of the solution, the salt concentrations, and the dissociation constants K_a . The pH of the solution measured by a pH meter was adjusted by adding NaOH. In the case of HSO₃⁻ and SO₃²⁻, the total concentration of S(IV) ([S(IV)] \equiv [SO₂(aq)] + [HSO₃⁻(aq)] + [SO₃²⁻(aq)]) was determined before and after each uptake measurement by iodometric titration.¹⁷ The concentration of each species was calculated using the first and second dissociation constants of H₂SO₃. The OH⁻ concentration was determined before and after each experiment by titration with standard sulfuric acid solution. The concentrations of anions of strong acids were taken to be the salt concentration in the solution.

Results

First-order loss rate coefficients of NO₃ due to uptake on aqueous solutions were measured by monitoring its concentration in the gas phase as a function of relative injector positions. A plot of \ln [NO₃] vs relative injector position was a line with a slope (cm⁻¹) of $-k_0$, from which the first-order rate coefficient, $k_m = k_0 v_g$ (s⁻¹), was calculated. Here, v_g is the gas flow velocity in the flow tube (cm s⁻¹). The measured value of k_m was corrected for the radial concentration gradient generated due to the uptake of NO₃ at the wall and to gas phase diffusion limitation to obtain k_c , the corrected first order rate coefficient, using the method developed by Brown.¹⁸ The diffusion coefficient of NO₃ in He was taken to be 370 and 100 Torr cm² s⁻¹ in H₂O vapor at 273 K.^{15,16}

The uptake coefficient γ was calculated from k_c :¹⁹

$$\gamma = (2r/\omega)k_c \quad (\text{I})$$

where ω is the average molecular speed of NO₃ (cm s⁻¹) and r is the effective flow-tube radius (0.925 cm). γ is related to the reactive loss in the liquid:^{20–23}

$$\frac{1}{\gamma} = \frac{1}{\alpha} + \frac{\omega}{4RTH\sqrt{D}k_i'} \quad (\text{II})$$

where α is the mass accommodation coefficient of NO₃ in water, R is the gas constant (0.082 L atm mol⁻¹ K⁻¹), T is the temperature (K), H is the Henry's law constant (M atm⁻¹), D is the diffusion coefficient of NO₃ in the solution (cm² s⁻¹), and k_i' is the first-order rate coefficient for NO₃ reaction in the solution (s⁻¹). Since the uptake of NO₃ onto the aqueous solution is limited by reactive loss in the solution, that is $\alpha \gg \gamma$, as previously reported,¹⁵ eq II is reduced to

$$\gamma^2 = (4RT/\omega)^2 H^2 D / k_i' \quad (\text{III})$$

In the aqueous phase, k_i' is given by¹⁵

$$k_i' = k_1' + k_i a_x \quad (\text{IV})$$

where k_1' is the first-order loss rate coefficient due to the reaction with water (reaction 1), k_i is the second-order rate coefficient

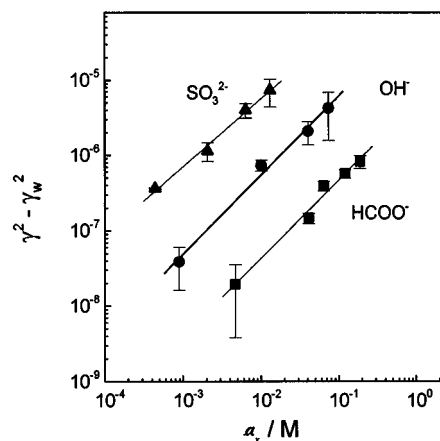


Figure 1. Plots of $\log(\gamma^2 - \gamma_w^2)$ as a function of $\log(a_x)$ for $X = \text{SO}_3^{2-}$ (solid triangles), OH^- (solid circles), and HCOO^- (solid squares). The error bars are 2σ precision only.

for the reaction with X^- ions (reaction i), and a_x is the activity of X^- ion. The activity is defined as the product of the concentration and the activity coefficients. The activity coefficients were taken from the literature where available.^{24,25} In the case of NaHSO₃ and Na₂SO₃, they were calculated using Debye–Huckel theory for dilute solutions. In pure water (reaction 1), the uptake coefficient γ_w determined¹⁵ to be $(2.0 \pm 0.5) \times 10^{-4}$ is given by

$$\gamma_w^2 = (4RT/\omega)^2 H^2 D / k_1' \quad (\text{V})$$

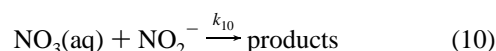
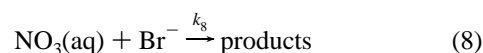
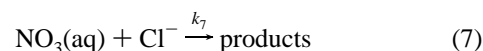
Combining eqs III–V, we obtain

$$\gamma^2 - \gamma_w^2 = (4RT/\omega)^2 H^2 D / k_i a_x \quad (\text{VIa})$$

Equation VIa can be rewritten as

$$\log(\gamma^2 - \gamma_w^2) = \log\{(4RT/\omega)^2 H^2 D / k_i\} + \log(a_x) \quad (\text{VIb})$$

If the uptake is limited by reactive loss in the bulk liquid phase, plots of $\log(\gamma^2 - \gamma_w^2)$ vs $\log(a_x)$ are expected to yield straight lines with slope equal to unity; $H^2 D / k_i$ is obtained from the intercept, i.e., when $a_x = 1$. As an example, plots of $\log(\gamma^2 - \gamma_w^2)$ vs $\log(a_x)$ for $X^- = \text{SO}_3^{2-}$, OH^- and HCOO^- are shown in Figure 1. The slopes of these plots were determined to be 0.9 ± 0.2 , 1.0 ± 0.2 , and 1.0 ± 0.2 for the reactions with SO_3^{2-} , OH^- , and HCOO^- ions, respectively. The quoted errors are 2σ (precision from unweighted fit to eq VIb). As expected, the slopes for reactants investigated here are ~ 1 , validating the assumption that the uptake of NO₃ onto an ionic solution is due to reactions in the bulk liquid phase and not on the surface of the flowing liquid. The values of $H^2 D / k_i$ for reactions 2–6 measured here are listed in Table 1 along with those for reactions 7–10 reported previously:^{15,16}



The quoted errors are 2σ and include both precision and estimated systematic errors, which are discussed below. The

TABLE 1: Rate Coefficients for Reactions of NO₃ with Several Ions

reaction (ion)	$H^2D/k_\gamma,^a$ M cm ² atm ⁻² s ⁻²	$k_\gamma/k_{7\gamma}$	$k_\gamma,^b$ M ⁻¹ s ⁻¹	$k_b,^c$ M ⁻¹ s ⁻¹ (273 K)
R2 (HSO ₃ ⁻)	$1.0_{-0.2}^{+0.3} \times 10^2$	$1.0_{-0.4}^{+0.5} \times 10^1$	2.9×10^7	7.2×10^8 LP, Exner <i>et al.</i> (1992)
R3 (SO ₃ ²⁻)	$6.5_{-1.9}^{+2.7} \times 10^1$	$6.5_{-2.7}^{+3.7}$	1.8×10^7	2.6×10^8 LP, Exner <i>et al.</i> (1992)
R4 (OH ⁻)	$7.7_{-2.7}^{+3.0}$	$7.7_{-3.6}^{+4.3} \times 10^{-1}$	2.1×10^6	4.1×10^7 LP, Exner <i>et al.</i> (1992)
R5 (HCOO ⁻)	$5.1_{-1.5}^{+2.0} \times 10^{-1}$	$5.1_{-2.1}^{+2.9} \times 10^{-2}$	1.4×10^5	2.6×10^7 LP, Exner <i>et al.</i> (1994)
R6 (CH ₃ COO ⁻)	$3.8_{-1.3}^{+1.5} \times 10^{-1}$	$3.8_{-1.7}^{+2.1} \times 10^{-2}$	1.1×10^5	9.1×10^5 LP, Exner <i>et al.</i> (1994)
R7 (Cl ⁻)	$1.0_{-0.3}^{+0.4} \times 10^1$	(reference)	2.8×10^6	2.8×10^6 LP, Exner <i>et al.</i> (1992) 2.7×10^7 PR, Kim and Hamill (1976) 2.2×10^7 PR, Neta and Huie (1986)
R8 (Br ⁻)	$3.6_{-1.1}^{+1.7} \times 10^2$	$3.6_{-1.5}^{+2.2} \times 10^1$	1.0×10^8	2.4×10^9 PR, Neta and Huie (1986)
R9 (I ⁻)	$1.7_{-0.4}^{+0.7} \times 10^4$	$1.7_{-0.6}^{+1.0} \times 10^3$	4.6×10^9	5.2×10^9 diffusion-controlled value
R10 (NO ₂ ⁻)	$6.7_{-1.9}^{+2.7} \times 10^2$	$6.7_{-2.8}^{+3.8} \times 10^1$	1.8×10^8	6.6×10^8 PR, Daniels (1969)

^a Errors are 2σ which include precision and systematic errors. (See text.) ^b Values were calculated using $k_7 = 2.8 \times 10^6$ M⁻¹ s⁻¹ at 273 K as a reference.¹³ (See text.) ^c Values at 273 K were calculated using the reported activation energies^{13,14} for reactions 2 and 4–7 and 16 kJ mol⁻¹ for reactions 3, 8, and 10. LP, laser photolysis; PR, pulsed radiolysis.

second-order rate coefficients for reactions 2–6 and 8–10 calculated by assuming $k_7 = 2.8 \times 10^6$ M⁻¹ s⁻¹ are also shown in Table 1. Therefore, we have implicitly assumed H^2D_γ to be $(3.6 \pm 1.0) \times 10^{-6}$ M² atm⁻² cm² s⁻¹, the value deduced in our previous work which also used $k_7 = 2.8 \times 10^6$ M⁻¹ s⁻¹.¹⁵

Discussion

Possible Sources of Errors in γ . In the present work, uncertainties in the water vapor pressure in the flow reactor, the diffusion coefficient of NO₃ in the gas phase, and simultaneous occurrence of gas and liquid phase reactions of NO₃ are the major sources of error in the measured values of γ . A change of pH at the surface of the liquid film due to uptake of NO₃ and N₂O₅ could be an additional source of error.

Water vapor in the flow reactor influences both the gas phase diffusion coefficients of NO₃ and the gas flow velocity in the reactor. We introduced He saturated with water vapor into the flow reactor to minimize evaporation and cooling of the liquid film. The temperature of the liquid film was measured by thermocouples at different locations along the liquid flow and was found to be the same within 1 K. The uncertainty in the water vapor pressure due to the uncertainty in the water temperature ($\Delta T = \pm 1$ K) is estimated to be within ± 0.3 Torr. For measurements of $\gamma \leq 3 \times 10^{-3}$, the error associated with the uncertainty in the water vapor pressure is estimated to be $\leq_{-9\%}^{+12\%}$. The asymmetry in the uncertainty is due to the nonlinear dependence of γ on water vapor pressure.

The pressure-dependent diffusion coefficient of NO₃, D_c , used in this work is estimated to be accurate to $\pm 20\%$ as reported previously.¹⁶ For low values of the uptake coefficient, i.e., $\gamma \leq 3 \times 10^{-3}$, an uncertainty in D_c of 20% translates to an uncertainty in γ of $\leq_{-15\%}^{+30\%}$. The estimated errors due to uncertainties in vapor pressure of water and D_c are conservative, and overall uncertainty in γ is estimated to be $\leq_{17\%}^{33\%}$.

NO₃ can also react with NO₂ in the reactor



N₂O₅ formed by reaction 11 could be lost on water at a (gas phase) diffusion-limited rate. Since the first-order rate coefficient k_g due to gas phase reactions is expected to be small as discussed below, the overall first-order rate coefficient for loss

of NO₃, k_{mp} , measured in the presence of gas phase reactions would be given by

$$k_{\text{mp}} = k_{\text{ma}} + k_g \quad (\text{VII})$$

where k_{ma} is the first-order rate coefficient of NO₃ loss measured in the absence of gas phase reactions and due only to uptake at the walls. In such a case, k_c used to obtain γ should be calculated using k_{ma} instead of k_{mp} . Otherwise, the gas phase loss would be included with the heterogeneous loss and lead to an overestimation of γ . Strictly, k_c is obtained numerically following the procedure discussed by Brown.¹⁸ As the value of k_g increases, the error introduced using expression VII would increase; for example, for $k_{\text{mp}} = 20$ s⁻¹, errors are $\sim 1\%$, $\sim 5\%$, and $\sim 10\%$ for $k_g = 1, 5,$ and 10 s⁻¹, respectively. A complete analysis, which includes corrections due to radial and axial concentration gradients as a result of the uptake at the wall and gas phase loss, needs to be performed when the contribution of k_g to the measured k_{mp} is large. Under our experimental conditions ($T = 273$ K, $P_{\text{total}} = 10$ – 17 Torr), the second-order rate coefficient for reaction 11 was measured to be 3×10^{-13} cm³ molecule⁻¹ s⁻¹.¹⁵ The concentration of NO₂ in the reactor is expected to be $\sim [\text{NO}_3]_0$, which is in the range of $(2$ – $20) \times 10^{11}$ molecule cm⁻³. Thus, the first-order rate coefficient of NO₃ loss due to reaction 11 must be < 1 s⁻¹. Therefore the error due to gas phase loss of NO₃ is estimated to be $\leq 30\%$ for $\gamma = 2 \times 10^{-4}$ and $\leq 5\%$ for $\gamma = 3 \times 10^{-3}$. The measured values of γ were independent of the initial NO₃ concentration; hence, the error in γ from the gas phase reaction is smaller than the precision in the measured γ values.

Another possible source of error is a pH change at the surface of the liquid due to the uptake of N₂O₅ formed by reaction 11 and the effect of this variation on measured values of γ . The concentration of a conjugate base (A⁻) of a weak acid (AH) is controlled by the pH of the aqueous solution via the equilibrium reaction



The ratio of activities of A⁻ and AH is obtained using the dissociation constant K_a of AH

$$a(\text{A}^-)/a(\text{AH}) = K_a/a(\text{H}^+) \quad (\text{VIII})$$

where a is the activity. The effective thickness of the liquid

surface for NO₃ uptake, l , is expressed by the diffusio-reactive length, $l = \sqrt{D/k'}$, and is much thinner than the thickness δ of the liquid film; e.g., $l = 10^{-5}$ cm for $D = 10^{-5}$ cm² s⁻¹ and $k' = 10^5$ s⁻¹ while $\delta = 0.025$ cm. Hence, the pH at the liquid surface must be known to estimate the effective concentration of A⁻. In this work, the pH at the liquid surface is likely to change due to the uptake of N₂O₅ to form HNO₃. To assess this contribution, the concentration of the NO₃⁻ ion in the water (3.5 L total volume) circulating through the reactor was measured by ion chromatography.¹⁵ After the circulating water was exposed to NO₃ for 3 h, the NO₃⁻ concentration in the solution was measured to be 3.2×10^{-5} M. The average formation rate of NO₃⁻ (and H⁺) in the liquid is, then, calculated to be $\sim 1 \times 10^{-8}$ mol s⁻¹. Under a plug flow approximation, the average H⁺ concentration [H⁺]_{s^{av}} at the liquid surface due to the uptake of N₂O₅ is estimated to increase by $\leq 3 \times 10^{-5}$ M. Estimation of the surface concentration is described in the Appendix. This increase is less than 10% of the concentrations of OH⁻ and SO₃²⁻ in the solution and less than 1% of HCOO⁻ and CH₃COO⁻ concentrations. Therefore, we conclude that such a pH change at the surface is negligible and does not change the ion concentration at the surface.

Comparison with Previous Studies. To place our measured relative rate coefficients for the NO₃ + X⁻ reactions on an absolute scale, we need at least one absolute rate coefficient. As reported in our previous publication,¹⁵ the absolute values of the rate coefficients, k_2 through k_{10} , were obtained from the measured H^2D/k and an extrapolation of Exner *et al.*'s value of $k_7 = 2.8 \times 10^6$ M⁻¹ s⁻¹ at 273 K.¹³ This rate coefficient leads to $H^2D/k = (3.6 \pm 1.0) \times 10^{-6}$ M² atm⁻² cm² s⁻¹. The measured relative values and those normalized to k_7 , given by Exner *et al.*, are listed in Table 1. For comparison, the rate coefficients measured in the bulk phase are also listed. Hereafter, the subscripts γ and b are used to distinguish between rate coefficients obtained from our uptake measurements and bulk phase data found in the literature.

Figure 2 shows a plot of $\log(k_\gamma)$ vs $\log(k_b)$ for reactions 2–10. The k_b values, when not available at 273 K, were calculated using the reported activation energies^{13,14} except for reactions 3 and 8–10. For reactions 3, 8, and 10, the activation energies have not been reported. However, our data show that the rate coefficients for these reactions are comparable to or larger than k_2 . The activation energy for reaction 2 was reported to be 16 kJ mol⁻¹,¹³ which is nearly the value of 20 kJ mol⁻¹ for the variation of the viscosity of water with temperature. Therefore, the activation energy (16 kJ mol⁻¹) for reaction 2 was used as those for reactions 3, 8, and 10. To our knowledge, k_b value for the reaction of NO₃ with I⁻ (reaction 9) is not measured. However, our data shows that this reaction is very fast. Therefore, we used diffusion-controlled rate coefficient, given by the expression²⁶

$$k_9 = 4\pi R^* D N_A \quad (\text{IX})$$

where R^* is some critical distance, D is the diffusion coefficient in the liquid phase, and N_A is Avogadro's number. R^* was assumed to be the sum of radii of I⁻ (2.2×10^{-8} cm)²⁶ and NO₃ (1.2×10^{-8} cm).¹⁵ D at 273 K was assumed to be the sum of the diffusion coefficients of I⁻ (1×10^{-5} cm² s⁻¹)²⁶ and NO₃ (1×10^{-5} cm² s⁻¹)¹⁵ in water.

In Figure 2, the solid line corresponds to $k_\gamma = k_b$. It is found that the k_γ values are smaller than the k_b values for most of the reactions studied here and that the value of $k_{9\gamma}$ is essentially diffusion-controlled. On the other hand, there is a linear correlation (dotted line in Figure 2) between $\log(k_\gamma)$ and $\log(k_b)$ when the reactions of NO₃ with HCOO⁻ (reaction 5), Cl⁻

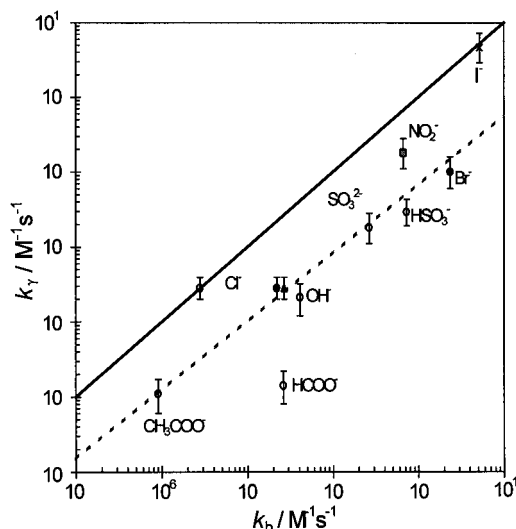


Figure 2. Plots of $\log(k_\gamma)$ as a function of $\log(k_b)$. k_γ 's were calculated using $H^2D/k = (3.6 \pm 1.3) \times 10^{-6}$ M² atm⁻² cm² s⁻¹. Values of k_b are from Daniels¹⁰ (pulsed radiolysis, solid square), Kim and Hamill¹¹ (pulsed radiolysis, solid triangle), Neta and Huie¹² (pulsed radiolysis, solid circles), and Exner *et al.*^{13,14} (laser photolysis study, open circles). Values of k_b at 273 K were extracted using the reported activation energies for the reactions with Cl⁻, HSO₃⁻, OH⁻, HCOO⁻, and CH₃COO⁻ ions^{13,14} and 16 kJ mol⁻¹ for the reactions with Br⁻, NO₂⁻, and SO₃²⁻ ions. For the reaction with I⁻, diffusion-controlled rate coefficient was used as k_{9b} . The solid line corresponds to $k_\gamma = k_b$ and the dotted line shows a linear correlation between $\log(k_\gamma)$ and $\log(k_b)$ with the exception of reactions of NO₃ with HCOO⁻, Cl⁻ (photolysis study), and I⁻.

(reaction 7, photolysis study), and I⁻ (reaction 9) ions are ignored. (Note: here we are comparing the measured rate coefficient for I⁻ with that calculated.) The slope of the line is 0.92 ± 0.23 (errors are 2σ and precision from unweighted fit only). Since the plot shown in Figure 2 is on log–log scale, the linear correlation does not depend on the rate coefficient of the reference reaction. The slope of ~ 1 indicates that $k_{i\gamma}$ is proportional to corresponding k_{ib} :

$$k_{i\gamma} = \text{constant} \times k_{ib} \quad (\text{X})$$

From the unweighted average of the ratios of $k_{ib}/k_{i\gamma}$, the proportionality constant was calculated to be 14 ± 8 where the error is 1σ and precision only. Therefore, it is possible that the NO₃ + Cl⁻ reaction is not a good choice for a reference reaction and all our rate coefficients are ~ 15 times smaller. If the rate coefficients are 15 times larger, our measured γ yields $H^2D/k = 2.5 \times 10^{-7}$ M² atm⁻² cm² s. However, such a low value for H^2D/k leads to other inconsistencies. For example, the value of $k_{9\gamma} = 6 \times 10^{10}$ M⁻¹ s⁻¹ is much larger than the estimated diffusion-controlled rate coefficient. Furthermore, the value of $k_{1\gamma} = 1.8 \times 10^4$ s⁻¹ is orders of magnitude larger than any reported first-order loss rate constant for loss of NO₃ in water.^{13,14,27} Therefore, it is not clear why this discrepancy between k_γ and k_b exists. A reliable rate coefficient for a reference reaction is essential. The possibility that there is an intrinsic reason for not measuring k_b in our experimental approach cannot be discounted even though the measured values of γ depend on the square root of k' , as is expected for a bulk phase reaction.

The larger disagreement between k_γ and k_b values for the reaction of NO₃ with HCOO⁻ (reaction 5) compared to other reactions discussed above is not understood. k_{5b} was measured by Exner *et al.* using laser photolysis.¹⁴ They also measured the rate coefficient for the reaction of NO₃ with undissociated

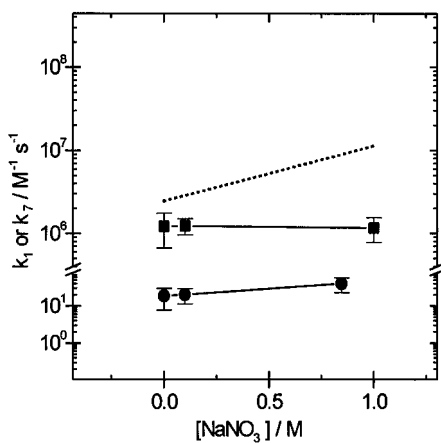


Figure 3. Plots of $k_{1\gamma}$ and $k_{7\gamma}$ as a function of $[\text{NaNO}_3]$ for the reactions of NO_3 with water (reaction 1) and Cl^- (reaction 7). Solid circles: $[\text{NaCl}] = 0 \text{ M}$. Solid squares: $[\text{NaCl}] = 1.2 \times 10^{-2} \text{ M}$. The error bars are 2σ precision only. The dotted line represents the effect of ionic strength on k_{7b} measured by Exner *et al.*¹³ The values of k_{7b} at 273 K were extracted using the reported activation energy.¹³

HCOOH at $\text{pH} = 0.5$, which is extrapolated to be $1.3 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$ at 273 K. Their rate coefficient for the reaction of NO_3 with HCOOH is close to the value of $k_{5\gamma}$ obtained in this work. However, the loss of NO_3 due to the reaction with HCOOH can be neglected in the pH range ($\text{pH} = 6.8\text{--}8.2$) maintained in our experiments. Furthermore, the pH change at the liquid surface was too small to form HCOOH . Hence, the reaction of NO_3 with HCOOH could not be important in our experiments.

The reason for the discrepancy between our relative rate coefficients and the absolute bulk phase liquid values is not clear. In our system, NO_3 was generated in the gas phase and was taken up by the reactions in the liquid phase just as in the atmospheric transfer of gas phase NO_3 to liquid droplets. In the absence of absolute rate coefficients in the liquid phase, our measured H^2D/k values can be used for atmospheric modeling.

Ionic Strength Effect (I) on γ . The rate coefficient for the reaction of NO_3 with Cl^- , k_{7b} , at room temperature was measured to be 7×10^7 and $1 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$ using pulsed radiolysis at high ionic strength ($I \geq 2 \text{ M}$)^{11,12} and $1 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$ using laser photolysis ($I = 0.11 \text{ M}$).¹³ Exner *et al.*¹³ attributed the discrepancy between the results of the pulsed radiolysis and laser photolysis studies to the effect of ionic strength on the rate coefficient. They reported that the reaction rate coefficients changed with ionic strength from $k_{7b} = 1 \times 10^7$ at $I = 0.11$ to $4.2 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$ at $I = 1 \text{ M}$.

The ionic strength effect observed by Exner *et al.*¹³ is large and should be detectable in our γ measurements. Therefore, the values of γ for reactions 1 and 7 were measured as a function of ionic strength by adding NaNO_3 to the solution. Since NO_3^- from NaNO_3 does not react with Na^+ or Cl^- , and the reaction of NO_3 with NO_3^- is merely a charge exchange, addition of NaNO_3 should not introduce any new loss processes for NO_3 . Since the viscosities of water and 1 M NaNO_3 solution at 293 K ($\eta/\eta_w = 1.06^{28}$) are essentially the same, the liquid phase diffusion coefficient of NO_3 at 273 K should also be constant. Using eqs III–V, the values of $H^2D/k_{1\gamma}$ and $H^2D/k_{7\gamma}$ were obtained. Plots of $k_{1\gamma}$ and $k_{7\gamma}$, calculated using $H^2D = 3.6 \times 10^{-6} \text{ M}^2 \text{ atm}^{-2} \text{ cm}^2 \text{ s}^{-1}$, against the concentration of NaNO_3 at two concentrations of added NaNO_3 are shown in Figure 3. Here we assume that the activity coefficient for Cl^- is not affected by the concentration of NaNO_3 (i.e., the ionic strength). Here, k_1 is defined as $k_1 = k_{1\gamma}/(a_{\text{H}_2\text{O}}/[\text{H}_2\text{O}])$. As can be seen in Figure

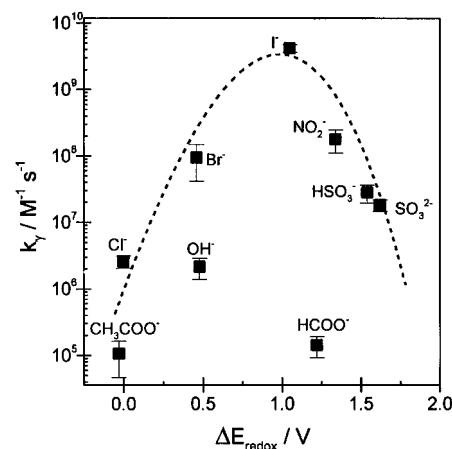
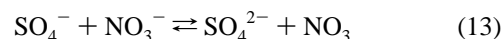


Figure 4. Plots of rate coefficients of NO_3 reactions, k_{γ} 's, against the difference of redox potentials of X/X^- and $\text{NO}_3/\text{NO}_3^-$ pairs. The broken line is merely a guide. Redox potentials of X/X^- are obtained from Rudich *et al.*¹⁵ for $\text{X}^- = \text{NO}_3$ and from Stanbury³⁶ for $\text{X}^- = \text{Cl}^-$, Br^- , I^- , NO_2^- , SO_3^{2-} , OH^- , and HCOO^- and from Exner *et al.*¹⁴ for $\text{X}^- = \text{HSO}_3^-$ and CH_3COO^- .

3, there is no visible effect of ionic strength on $k_{1\gamma}$ and $k_{7\gamma}$. The reason for the disagreement between our results and those of Exner *et al.*¹³ is not understood.

Reaction Mechanism. The reactions of NO_3 with anions studied in this work are believed to be electron transfer processes.^{13,14} The rate coefficient for outer-sphere electron transfer is known to depend on the difference in Gibbs free energy between the reactant and the product,²⁹ which is proportional to ΔE_{redox} , the difference in the redox potentials of X/X^- and $\text{NO}_3/\text{NO}_3^-$ pairs. Figure 4 shows a plot of $\log(k_{\gamma})$ as a function of ΔE_{redox} . As can be seen in the figure, for $\Delta E_{\text{redox}} < 1 \text{ V}$, the rate coefficients increase with increasing ΔE_{redox} . On the other hand, for $\Delta E_{\text{redox}} > 1 \text{ V}$, the rate coefficients decrease with increasing ΔE_{redox} . This overall feature (parabolic behavior) seen in Figure 4 is qualitatively consistent with Marcus theory for electron transfer reactions.²⁹

The redox potential of $\text{SO}_4^-/\text{SO}_4^{2-}$ pair is calculated to be 0.02 V lower than that of $\text{NO}_3/\text{NO}_3^-$ pair from the measured rate coefficients for the forward and reverse reactions^{13,30}



The $\text{SO}_4^- + \text{X}^-$ reactions are believed to be electron transfer processes.³¹ Therefore, we expect a correlation between SO_4^- radical reactions and those of NO_3 . The rate coefficients for the NO_3 reactions determined here are compared to those for corresponding SO_4^- reactions, $k_b(\text{SO}_4^-)$, in Figure 5. Because the rate coefficients for $\text{SO}_4^- + \text{X}^-$ reactions at 273 K are not available, the values at room temperature were used.^{32,33} With the exception of HCOO^- and I^- reactions, a linear correlation between NO_3 and SO_4^- reaction rate coefficients is observed. The slope of the line is 1.2 ± 0.4 (error is 2σ precision derived from unweighted fit). This slope of near unity suggests that NO_3 and SO_4^- have similar reactivity toward X^- ions and the mechanism for $\text{NO}_3 + \text{X}^-$ reaction is an electron transfer process.

Atmospheric Implications. From the present and previously reported data, the reactive uptake coefficient, γ , of the NO_3 radical on water droplets with several dissolved ionic species can be calculated using the expression $\gamma^2 = \gamma_w^2 + (4RT/\omega)^2 \sum_i H^2D/k_i[\text{X}^-]$. For a cloud droplet with $[\text{Cl}^-] = 1 \times 10^{-4} \text{ M}$, $[\text{S(IV)}] = 1 \times 10^{-6} \text{ M}$, $[\text{HCOOH} + \text{HCOO}^-] = 5 \times 10^{-6} \text{ M}$, $[\text{CH}_3\text{COOH} + \text{CH}_3\text{COO}^-] = 2 \times 10^{-6} \text{ M}$, and $\text{pH} = 5.0$,^{6,7,9} γ is estimated to be 2.2×10^{-4} . In this case, NO_3 is lost mostly

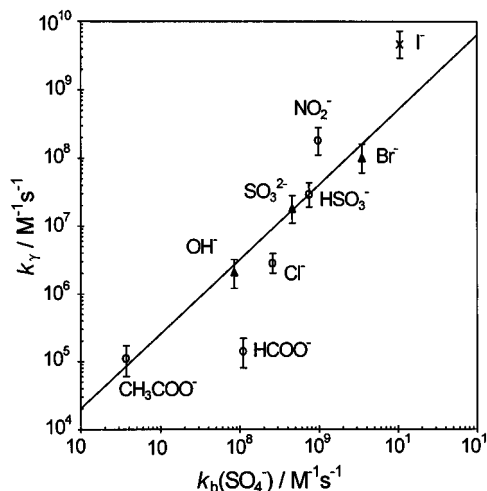
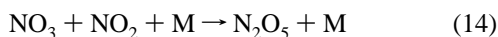
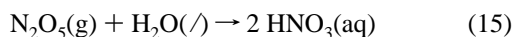


Figure 5. Comparison between rate coefficients of NO₃ reactions, k_y 's, obtained at 273 K in this work and those for corresponding SO₄²⁻ reactions measured in the bulk at 298 K. Values of $k_b(\text{SO}_4^-)$ are obtained from Neta *et al.*³² (solid triangles) and Wine *et al.*³³ (open circles). For reaction with I⁻, calculated diffusion-controlled rate coefficient is used as $k_{9b}(\text{SO}_4^-)$ (cross). The error bars include precision and systematic errors. The solid line shows a linear correlation between $\log(k_y)$ and $\log(k_b(\text{SO}_4^-))$ excluding the reactions with HCOO⁻ and I⁻ ions.

via reaction with H₂O, reaction 1. If the concentration of [S(IV)] were an order of magnitude higher, reaction with HSO₃⁻ would be competing with reaction 1. The reactions with HCOO⁻ (reaction 9) and CH₃COO⁻ (reaction 10) at the above concentrations would have negligible contribution to the NO₃ loss rate constant. For a cloud with 40 droplets cm⁻³ of 3 × 10⁻³ cm diameter droplets,⁷ NO₃ lifetime due to heterogeneous loss will be ~500 s. This estimated lifetime is comparable to or shorter than that due to the loss via uptake of N₂O₅:



followed by



Therefore, reactive uptake of NO₃ onto clouds would have an impact on the concentration of NO₃ in the gas phase.

The reactive uptake of NO₃ is important not only for the NO₃ loss in the gas phase but also for the oxidation of species in the solution. For example, reactions 9 and 10, while they are a minor contributor to NO₃ loss, are sink processes for HCOO⁻ and CH₃COO⁻ ions in droplets during the night. They generate HCOO and CH₃COO radicals which instantly decompose to give H + CO₂ and CH₃ + CO₂, respectively. Thus, they will destroy the acids and generate new radicals. The uptake of NO₃ can also initiate the catalytic oxidation of S(IV) to S(VI), both directly and indirectly, in clouds.³⁴

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Appendix

The average concentration of H⁺, [H⁺]_s, in the liquid surface (thickness $l = (D/k')^{1/2}$) formed due to the uptake of N₂O₅ was estimated using the plug flow approximation. To simplify our argument, we assume that gaseous N₂O₅ is introduced into

the reactor through the injector at $z = 0$ and is taken up into water with $\gamma = 1$, which results in the conversion into 2(H⁺ + NO₃⁻).

It is assumed that N₂O₅ decays due to the uptake into water with a gas phase diffusion-limited rate coefficient k_{dl} , which is estimated to be 42 s⁻¹ ($P_{\text{total}} = 13.5$ Torr) using the diffusion coefficients of 290 and 64 Torr cm² s⁻¹ for N₂O₅ in He and in H₂O, respectively.^{22,35} In the flow reactor, the gas-liquid contact time, $t_c (=L/v_g)$, where v_g is the flow velocity of liquid film), below the injector (reaction length $L \sim 30$ cm) is ~3 s. The total number of N₂O₅ molecules taken up after introduction into the reactor through the injector, $N_{\text{N}_2\text{O}_5}^{\text{T}}$, is calculated by

$$N_{\text{N}_2\text{O}_5}^{\text{T}} = J_0 \{1 - \exp(-k_{\text{dl}}L/v_g)\} t_c \quad (\text{AI})$$

where J_0 is the flux of N₂O₅ into the gas phase through the injector and v_g is the gas flow velocity. The average formation rate of H⁺ + NO₃⁻ was calculated to be ~1 × 10⁻⁸ mol s⁻¹. This means that, during the contact time, 3 × 10⁻⁸ mol of H⁺ ions is formed, which must correspond to the amount of 2N₂O₅^T. Using the typical values of k_{dl} (42 s⁻¹) and v_g (850 cm s⁻¹), J_0 is calculated to be 6.7 × 10⁻⁹ mol s⁻¹.

The number of N₂O₅ molecules taken up into water (surface area = 2πr δz) per unit time at $z = (Z' - \delta z) \sim Z'$ downstream the injector is given by

$$\Delta J_{\text{N}_2\text{O}_5}(Z') = J_0 \exp(-k_{\text{dl}}Z'/v_g)(k_{\text{dl}}/v_g) \delta z \quad (\text{AII})$$

Because of the rapid hydrolysis of N₂O₅, H⁺ is immediately formed at the surface. The number of H⁺ formed at the surface due to the uptake of N₂O₅ is given by

$$N_0(Z') = 2\Delta J_{\text{N}_2\text{O}_5}(Z')(\delta z/v_g) \quad (\text{AIII})$$

Protons formed at $z = Z'$ diffuse into the bulk while the liquid film flows down the reactor, and at $z = Z$ the concentration profile of H⁺ formed at $z = Z'$, $C'(x, Z')$, is given as a function of the distance x from the surface:²⁶

$$C'(x, Z') = \frac{N_0(Z')}{A\sqrt{\pi D_f t}} \exp\left(-\frac{x^2}{4D_f t}\right) \quad (\text{AIV})$$

where $t = (Z - Z')/v_f$ and $A = 2\pi r \delta z$. The concentration $C(x, Z)$ of H⁺ at $z = Z$ is obtained by integrating the contribution of H⁺ injected at $z = 0$ to Z ,

$$C(x, Z) = \lim_{\delta z \rightarrow 0} \int_0^{Z-\delta z} C'(x, Z') dZ' \quad (\text{AV})$$

The average H⁺ concentration in the liquid surface with the thickness of l at $z = Z$, [H⁺]_s^{av}(Z), is given by

$$[\text{H}^+]_s^{\text{av}}(Z) \leq C(x=0, Z) \quad (\text{AVI})$$

In our calculation, δz was assumed to be $\leq l \times 10^{-2}$ (for $l = 10^{-3}$ – 10^{-7} cm), which corresponds to a shorter mixing time than the reaction time of NO₃ in the liquid. Using the typical values, i.e., $J_0 = 6.7 \times 10^{-9}$ mol s⁻¹, $v_g = 850$ cm s⁻¹, $v_f = 10$ cm s⁻¹, and $D_f = 10^{-5}$ cm² s⁻¹ for NO₃ and H⁺, [H⁺]_s^{av}(Z) was obtained to be $\leq 3 \times 10^{-5}$ M.

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